



PDHonline Course M167 (3 PDH)

Steam Management - Overview of Steam Traps

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Steam Management – Overview of Steam Traps

Course Content

A steam trap is a valve device that discharges condensate and air from the line or piece of equipment while not permitting the escape of live steam. The three most important functions of steam traps are:

- To discharge condensate as soon as it is formed
- Not to allow steam to escape.
- To be capable of discharging air and other non-condensable gases.

Types of Steam Traps

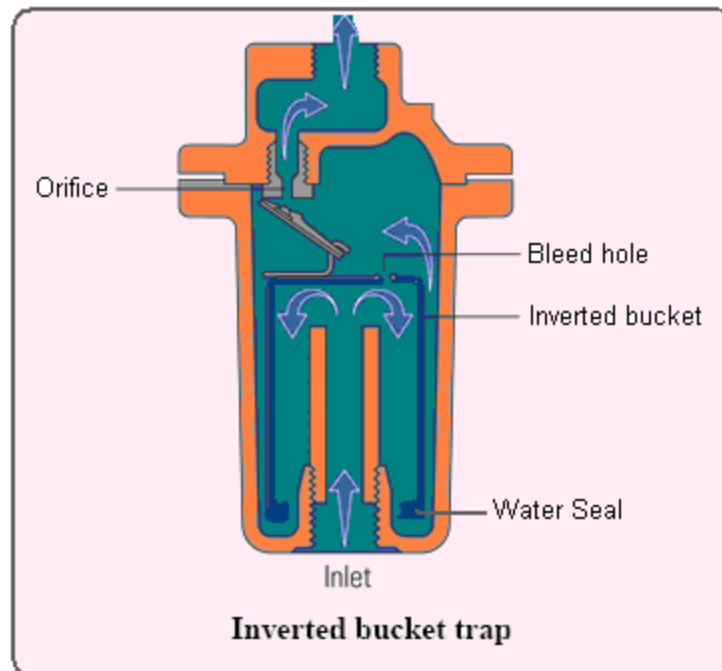
There are three basic types of steam trap into which all variations fall; all three are classified by International Standard ISO 6704:1984.

Group	Principle	Sub-group
<i>Mechanical Trap</i>	This range of steam traps operates by sensing the difference in density between steam and condensate.	Bucket type <ul style="list-style-type: none">• Open bucket• Inverted bucket with lever, without lever Float type <ul style="list-style-type: none">• Float with lever• Free float
<i>Thermodynamic Trap</i>	This range of steam traps operate by sensing difference in thermodynamic properties between steam and condensate. Thermodynamic steam traps rely on the fact that hot condensate, released under dynamic pressure, will flash-off to give a mixture of steam and water.	Disc type Impulse type Labyrinth type Orifice type
<i>Thermostatic Trap</i>	This range of steam traps operate by sensing difference in temperature between steam and condensate.	Bimetallic type Metal expansion type

Some of the important traps in industrial use are discussed below

Inverted Bucket Steam Trap

The inverted bucket trap is a mechanically actuated model that uses an upside down bucket as a float. The bucket, connected to an outlet valve through a mechanical linkage, sinks when condensate fills the steam trap, opening the outlet valve. The bucket floats when steam enters the trap, closing the valve.



Advantages of the inverted bucket steam trap

- 1) The inverted bucket trap can be a very economical solution for low-to-medium pressures applications such as plant heating and light-duty processes. When handling high pressures and capacities, these traps become large and expensive.
- 2) Like a float-thermostatic steam trap, it has a good tolerance to water hammer conditions
- 3) Can be used on superheated steam lines with the addition of a check valve on the inlet
- 4) Failure mode is usually open, so it's safer on those applications that require this feature, for example turbine drains

Disadvantages of the inverted bucket steam trap

- 1) The small size of the hole in the top of the bucket means that this type of trap can only discharge air very slowly. The hole cannot be enlarged, as steam would pass through too quickly during normal operation.
- 2) Inverted bucket traps, as a group, are capable of handling a wide range of steam pressures and condensate capacities. However, each specific steam trap handles a very narrow range.

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An inverted bucket trap designed for 8.5 Kg/cm² service operates at pressures below this;

however, its capacity is so diminished that it may “back up” a system with unwanted condensate.

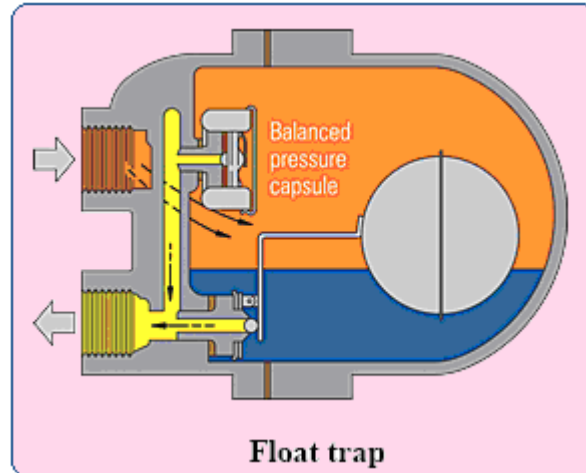
- 3) There should always be enough water in the trap body to act as a seal around the lip of the bucket. If the trap loses this water seal, steam can be wasted through the outlet valve. This can often happen on applications where there is a sudden drop in steam pressure, causing some of the condensate in the trap body to ‘flash’ into steam. The bucket loses its buoyancy and sinks, allowing live steam to pass through the trap orifice. Only if sufficient condensate reaches the trap will the water seal form again, and prevent steam wastage.

Important Guidelines for Inverted Bucket Traps

- 1) If an inverted bucket trap is used on an application where pressure fluctuation of the plant can be expected, a check valve should be fitted on the inlet line in front of the trap. Steam and water are free to flow in the direction indicated, while reverse flow is impossible as the check valve would be forced onto its seat.
 - 2) The higher temperature of superheated steam is likely to cause an inverted bucket trap to lose its water seal. A check valve in front of the trap should be regarded as essential under such conditions. Some inverted bucket traps are manufactured with an integral check valve as standard.
 - 3) The inverted bucket trap is likely to suffer damage from freezing, if installed in an exposed position with sub-zero ambient conditions. Suitable insulation lagging can overcome this problem, if conditions are not too severe. If ambient conditions well below zero are to be expected, then it may be prudent to consider a more robust type of trap to do the job. *In the case of mains drainage, a thermodynamic trap would be the first choice.*
 - 4) It is important to correlate the pressure rating and size with a specific application. For example, an inverted bucket trap designed for up to 1 kg/cm² service fails to operate at pressures above 1 kg/cm².
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Float and Thermostatic Steam Trap

The ball float type trap operates by sensing the difference in density between steam and condensate. The float and thermostatic (F&T) trap is a hybrid. As condensate collects, it lifts a float which opens a valve as much as required. A built-in thermostatic element purges air and other non-condensable gases and closes off when steam enters the trap. This type of trap continuously drains the condensate as it forms.



Advantages of the float-thermostatic steam trap

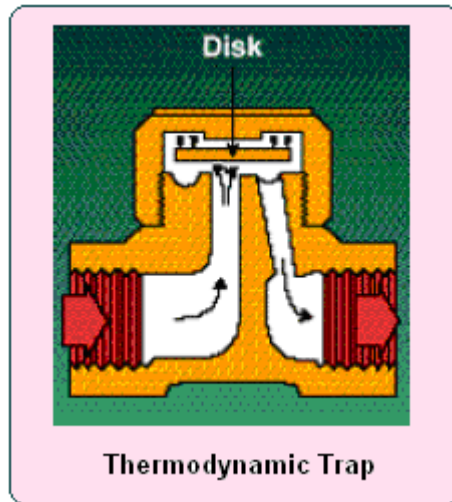
- 1) *The trap continuously discharges condensate as soon as it is formed. This makes it the first choice for applications where the rate of heat transfer is high for the area of heating surface available.*
- 2) The F&T trap is able to purge the system of air and other non-condensable gases, allowing for quick system startups.
- 3) It is able to handle heavy or light condensate loads equally well and is not affected by wide and sudden fluctuations of pressure or flowrate.
- 4) The float valve with thermostatic air vent is resistant to water hammer and has large capacity of its size.

Disadvantages of the float-thermostatic steam trap

- 1) Although less susceptible than the inverted bucket trap, the float type trap can be damaged by severe freezing and the body should be well lagged, and / or complemented with a small supplementary thermostatic drain trap, if it is to be fitted in an exposed position.
- 2) As with all mechanical type traps, different internals are required to allow operation over varying pressure ranges. Traps operating on higher differential pressures have smaller orifices to balance the buoyancy of the float.
- 3) This type of trap is vulnerable to dirt in the system and the float ball can get damaged by severe water hammer.
- 4) Similar to the inverted bucket trap, the F&T design handles a wide range of steam pressures and condensate loads, in a group system. However, each individual trap can only handle a very narrow range of pressures and capacities, making it critical to exactly correlate the pressure rating and size to the application.

Thermodynamic Steam Trap

The thermodynamic trap has a simple mode of operation. The trap operates by means of the dynamic effect of flash steam as it passes through the trap. Thermodynamic or disk traps are designed with a flat disk which moves between a cap and seat. On startup, condensate flow raises the disk and opens the discharge port. When steam or very hot condensate arrives, it closes the disk, which stays closed as long as pressure is maintained above the disk. Heat radiates out through the cap, which diminishes the pressure over the disk, opening the trap to discharge condensate.



The rate of operation depends on steam temperature and ambient conditions. Most traps will stay closed for between 20 and 40 seconds. If the trap opens too frequently, perhaps due to a cold, wet, and windy location, the rate of opening can be slowed by simply fitting an insulating cover onto the top of the trap.

Advantages of the thermodynamic steam trap

- 1) Thermodynamic traps can operate across their entire working range without any adjustment or change of internals.
- 2) Thermodynamic traps are relatively small and compact for the amount of condensate they are capable of discharging.
- 3) Thermodynamic traps can be used on high pressure and superheated steam and are not affected by water hammer or vibration.
- 4) *Thermodynamic traps are not damaged by freezing and are unlikely to freeze*, if installed with the disc in a vertical plane and discharging freely to atmosphere. However, operation in this position may result in wear of the disc edge.
- 5) As the disc is the only moving part, maintenance can easily be carried out without removing the trap from the line.

- 6) The audible 'click' which occurs as the trap opens and closes makes trap testing very straight forward.

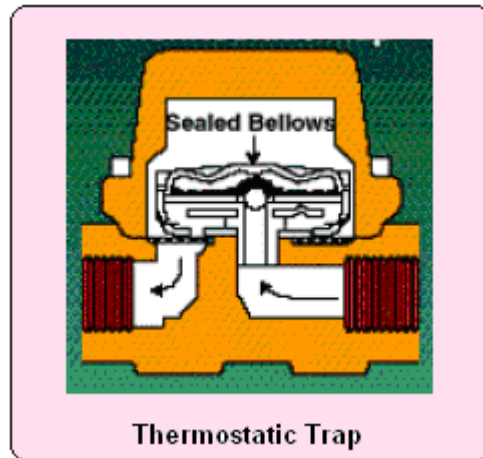
Disadvantages of the thermodynamic steam trap

- 1) Thermodynamic traps can discharge a large amount of air on start-up, if the inlet pressure builds up slowly. However, rapid pressure build-up will cause high velocity air to shut the trap in the same way as steam, and it will 'air-bind'. In this case a separate thermostatic air vent can be fitted in parallel with the trap.
 - 2) The primary disadvantage is difficulty in discharging air and other non-condensable gases during rapid pressure build-up. The thermodynamic steam traps are though available with an inbuilt anti-air-binding disc, which prevents air pressure building up on top of the disc and allows air to escape.
 - 3) Wear and dirt can be a problem with a disk trap because of the large, flat seating surfaces involved. If pressure is not maintained above the disk, the trap cycles frequently, wastes steam, and fails prematurely.
 - 4) Thermodynamic steam traps will not work positively on very low differential pressures.
 - 5) The discharge of the trap can be noisy and this factor may prohibit the use of a thermodynamic trap in noise sensitive areas. A diffuser may be needed to attenuate the discharge noise.
 - 6) Care should be taken not to oversize a thermodynamic trap as this can increase cycle times and induce wear.
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Thermostatic Steam Trap

Thermal element thermostatic traps are temperature actuated. On startup the thermal element is in a contracted position with the valve wide open purging air, condensate and other non-condensable gases.

As the system warms up, heat generates pressure in the thermal element, causing it to expand and throttle the flow of hot condensate through the discharge valve. When steam follows the hot condensate into the trap, the thermal element fully expands, closing the trap. If condensate enters the trap during system operation, it cools the element, contracting it off the seat, and quickly discharging condensate. Thermostatic traps can have either continuous or intermittent discharge depending upon the load.



Thermostatic traps are often considered a universal steam trap and are small, lightweight, and compact. For light-to-moderately high condensate loads, thermostatic steam traps offer advantages in terms of initial cost, long-term energy conservation, reduced inventory, and ease in application and maintenance.

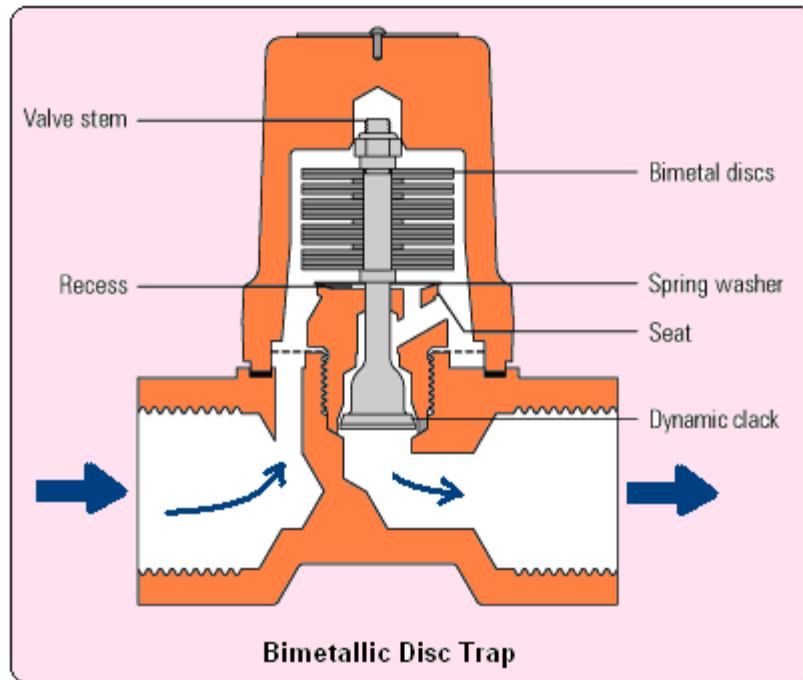
Single trap can operate over extremely broad pressure and capacity ranges. Thermal elements can be selected to operate within a range of steam temperatures. In steam tracing applications it may be desirable to actually back up hot condensate in the lines to extract its thermal value.

These are normally not recommended for extremely high condensate requirements (over 7000 kg/hr).

The biggest disadvantage of the thermostatic traps is that these retain condensate until cooled to below saturation temperature. Should this condensate remain in the steam space, it would reduce the heat transfer area and the heater performance.

Bimetallic Steam Trap

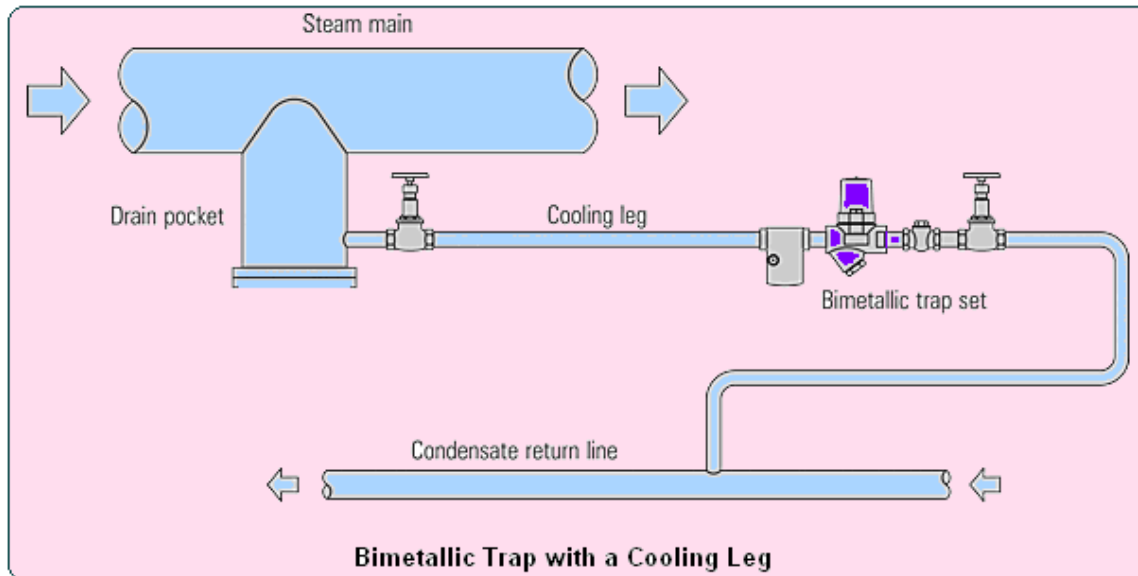
Bimetallic steam traps operate on the same principle as a heating thermostat. A bimetallic strip or wafer connected to a valve bends or distorts when subjected to a change in temperature. When properly calibrated, the valve closes off against a seat when steam is present, and opens when condensate, air, and other non-condensable gases are present.



There are two important points to consider regarding this simple element:

1. Operation of the steam trap takes place at a certain fixed temperature, which may not satisfy the requirements of a steam system possibly operating at varying pressures and temperatures.
2. Because the power exerted by a single bimetal strip is small, a large mass would have to be used which would be slow to react to temperature changes in the steam system.

A simple bimetal element tends to react to temperature changes in a linear fashion. The condensate is discharged below steam temperature, which shall cause water logging of the steam space unless the steam trap is fitted at the end of a long cooling leg (typically 1-3 meter of unlagged pipe). The figure below shows the general arrangement.



The flash steam produced whenever condensate is discharged from a higher to a lower pressure will tend to cause an increase in backpressure in the condensate line. The cooling leg allows the condensate to cool down, producing less flash steam in the condensate line and thus helping to reduce the backpressure.

The condensate is discharged at varying temperatures below saturation temperature. The maximum energy from the condensate is extracted before it drains to waste, and this is why these traps are used on tracer lines where condensate is often dumped to waste.

Bimetallic steam traps are not suitable for fitting to process plants where immediate condensate removal is vital for maximum output to be achieved. This is particularly relevant on temperature controlled plants.

Advantages of the bimetallic steam trap:

- 1) Advantages are their relatively small size for the condensate loads they handle.
- 2) Bimetallic steam traps are usually able to withstand water hammer, corrosive condensate, and high steam pressures.
- 3) The valve is wide open when the steam trap is cold, giving good air venting capability and maximum condensate discharge capacity under 'start-up' conditions.
- 4) As condensate tends to drain freely from the outlet, this type of steam trap will not freeze up when working in an exposed position.
- 5) The bimetal elements can work over a wide range of steam pressures without any need for a change in the size of the valve orifice.
- 6) Maintenance of this type of steam trap presents few problems, as the internals can be replaced without removing the trap body from the line.

Disadvantages of the bimetallic steam trap:

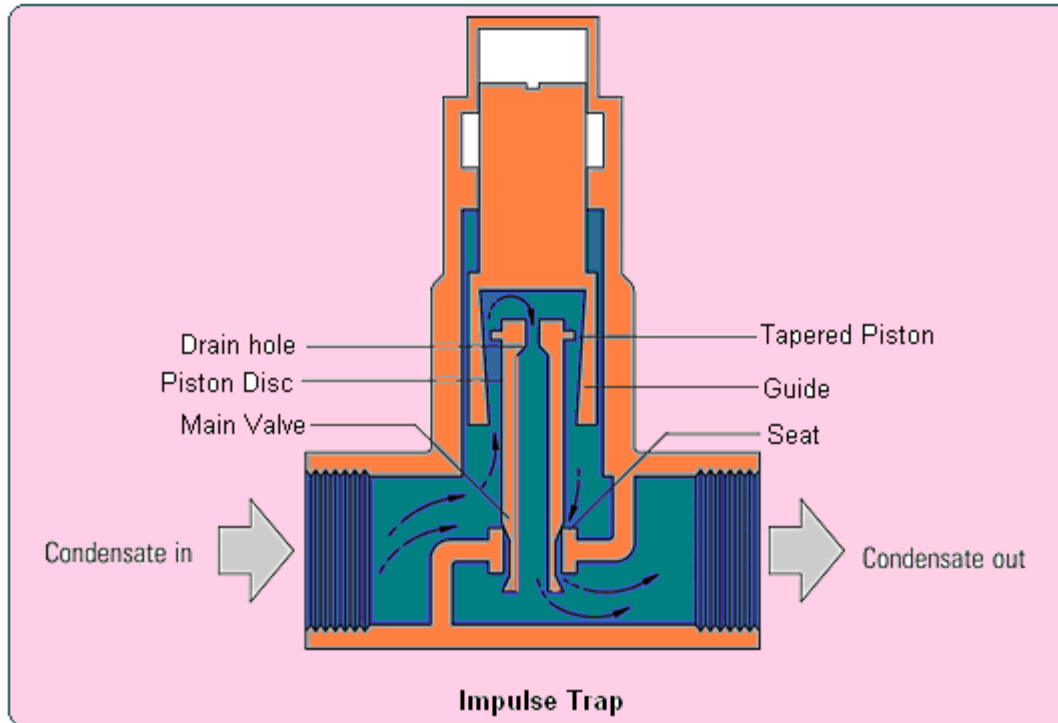
- 1) A disadvantage is that the traps must be set, generally at the plant, for a particular steam operating pressure. If the trap is used for a lower pressure, it may discharge live steam. If used at a higher steam pressure, it can back up condensate into the system.
 - 2) Bimetallic steam traps do not respond quickly to changes in load or pressure because the element is slow to react.
 - 3) Some bimetallic steam traps are vulnerable to blockage from pipe dirt due to low internal flow velocities.
 - 4) If the bimetallic steam trap has to discharge against a significant backpressure, the condensate must cool to a lower temperature than is normally required before the valve will open. A 50% backpressure may cause up to a 50°C drop in discharge temperature. It may be necessary to increase the length of cooling leg to meet this condition.
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Impulse Steam Trap

The impulse trap as shown in figure below is a category of thermodynamic trap.

As the condensate approaches steam temperature some of it flashes to steam as it passes through the gap. It creates an intermediate pressure on the piston disc, which effectively positions the main valve to meet the load. Increasing flow of air and condensate will act on the piston disc and lift the main valve off its seat to give increased flow. Some condensate will also flow through the gap between the piston and disc, through the seat and away to the trap outlet.

The trap can be adjusted by moving the position of piston relative to the seat, but the trap is affected by significant backpressure. Impulse traps cannot give a dead tight shut-off and therefore the use of impulse traps is relatively limited as compared to other types available.



Advantages of the impulse steam trap

- 1) Impulse traps have a substantial condensate handling capacity for their size.
- 2) They will work over a wide range of steam pressures without any change in valve size and can be used on high pressure and superheated steam.
- 3) They are good at venting air and cannot 'air-bind'.

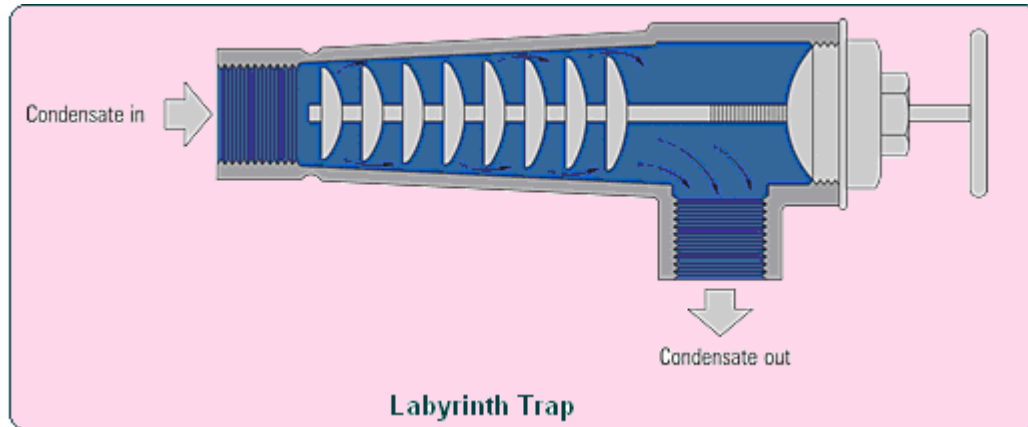
Disadvantages of the impulse steam trap

- 1) Impulse traps cannot give a dead tight shut-off and will blow steam on very light loads.
- 2) They are easily affected by any dirt which enters the trap body due to the extremely small clearance between the piston and the cylinder.
- 3) The traps can pulsate on light load causing noise, water hammer and even mechanical damage to the valve itself.
- 4) They will not work against a backpressure which exceeds 40% of the inlet pressure.

Labyrinth Steam Trap

A simple form of the labyrinth trap belongs to thermodynamic category. It consists of a series of baffles which can be adjusted by means of a hand wheel. Hot condensate passing between the first baffle and the trap body is subject to a drop in pressure and some of it 'flashes' to steam. The

space around the next baffle has to cope with an increased volume of hot condensate and prevents the escape of live steam. The baffle plates can be moved either in or out using the hand wheel, which alters their position relative to the body, effectively altering the overall size of the orifice.



Advantages of the labyrinth steam trap

This type of trap is comparatively small in relation to its capacity and there is little potential for mechanical failure since there are no automatic parts.

Disadvantages of the labyrinth steam trap

The labyrinth trap has to be adjusted manually whenever there is a significant variation in either steam pressure or condensate load. If the setting is not right for the prevailing conditions, steam wastage or water logging of the steam space will occur (like a fixed orifice trap).

Fixed Orifice Steam Trap

These are devices containing a hole of predetermined diameter to allow a calculated amount of condensate to flow under specific pressure conditions. In practice, condensate loads and steam pressures can vary considerably between start-up and running loads, for example,

- If sized on running load, fixed orifice traps will waterlog on start-up, reducing plant performance over this period, increasing start-up times and the risk of corrosion.
- If sized on start-up load, fixed orifice traps will waste steam when the plant is running, and increase start-up times.

Fixed orifice traps often block with dirt due to the small size of orifice and are not recommended.

Considerations for Steam Trap Selection

The trap selection follows on the basis that the requirements of pressure, condensate load and air venting.

Air venting: At 'start-up', the heater space is filled with air, which unless displaced, will reduce heat transfer and increase the warm-up time. It is important to purge air as quickly as possible before it has a chance to mix with the incoming steam, otherwise it could increase production times, warm-up times and corrosion.

Separate air vents may be required on larger or more awkward steam spaces, but in most cases air in the system is discharged through the steam traps. *Here thermostatic traps have a clear advantage over some types of trap since they are fully open at start-up.* Float traps with inbuilt thermostatic air vents are useful, while many thermodynamic traps are also quite capable of handling moderate amounts of air. However, the small hole in fixed orifice condensate outlets and the bleed hole in inverted bucket traps vent air slowly.

Condensate removal: Having vented the air, the trap must then pass the condensate but not the steam. Leakage of steam at this point is inefficient and uneconomical. The steam trap has to allow condensate to pass whilst trapping the steam in the process. If good heat transfer is critical to the process, then condensate must be discharged immediately and at steam temperature. Water logging is one of the main causes of inefficient steam plant as a result of incorrect steam trap selection.

Temperatures & Pressures: Before choosing a particular steam trap, it is necessary to consider the needs of the process. The quantity of condensate a steam trap has to deal with may vary considerably. It may have to discharge condensate at steam temperature (i.e. as soon as it forms in the steam space) or it may be required to discharge below steam temperature, giving up some of its 'sensible heat' in the process.

Steam traps may be subjected to extremes of temperature or even water hammer. The pressures at which steam traps can operate may be anywhere from vacuum to well over a hundred bar. To suit these varied conditions there are various choices, each having their own advantages and disadvantages. Experience shows that steam traps work most efficiently when their characteristics are matched to that of the application.

It is imperative that the correct trap is selected to carry out a given function under given conditions. Whatever the conditions, correct steam trap selection is important to system efficiency. Check with suppliers for your type of application. A table below gives general guidelines.

Application	Feature	Suitable Trap
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Application	Feature	Suitable Trap
Steam Mains	<ul style="list-style-type: none">- Open to atmosphere, small capacity- Frequent change in pressure- Low pressure – high pressure	<ul style="list-style-type: none">• Thermodynamic Type
<ul style="list-style-type: none">• Equipment• Reboiler• Heater• Dryer• Heat exchanger etc	<ul style="list-style-type: none">- Large Capacity- Variation in temperature and pressure is undesirable- Efficiency of the equipment is a problem	<ul style="list-style-type: none">• Mechanical Type• Inverted Bucket• Float Type
<ul style="list-style-type: none">• Tracer line• Instrumentation	<ul style="list-style-type: none">- Reliability with no overheating	<ul style="list-style-type: none">• Thermodynamic Type• Bimetallic Type

Plant performance: When the basic requirements of removing air, condensate and pressures have been considered, attention may be turned to 'plant performance'. Simply put, unless specifically designed to waterlog, for a heat exchanger to operate at its best performance, the steam space must be filled with clean dry steam. The type of steam trap will influence this. *For instance, thermostatic traps retain condensate until cooled to below saturation temperature. Should this condensate remain in the steam space, it would reduce the heat transfer area and the heater performance.* The discharge of condensate at the lowest possible temperature may seem very attractive, but generally most applications require condensate to be removed from the steam space at steam temperature. This needs a steam trap with different operating properties to the thermostatic type, and this usually means either a mechanical or thermodynamic type trap. Once chosen, it is necessary to size the steam trap. This will be determined by the system conditions and process parameters such as:

- Maximum steam and condensate pressures
- Operating steam and condensate pressures
- Temperatures and flow rates
- Whether the process is temperature controlled.

System Design Considerations & Installation Aspects

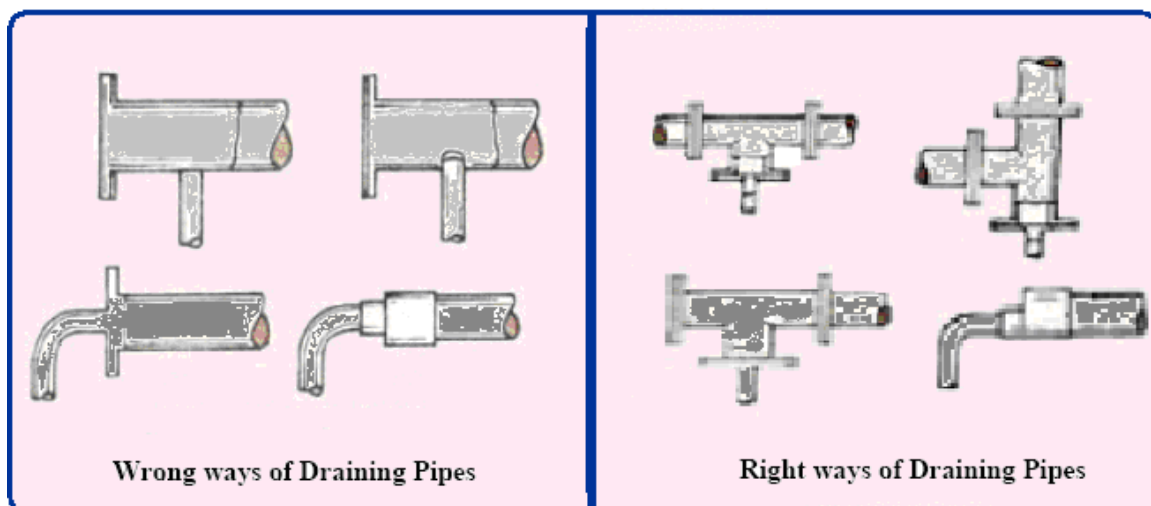
In most cases, trapping problems are caused by bad installation rather than by the choice of the wrong type or faulty manufacture. To ensure a trouble-free installation, careful consideration

should be given to the drain point, pipe sizing, air venting, steam locking, group trapping vs. individual trapping, dirt, water hammer, lifting of the condensate, etc.

Drain Point

The drain point should be so arranged that the condensate can easily flow into the trap. This is not always appreciated. For example, it is useless to provide a 15mm drain hole in the bottom of a 150 mm steam main, because most of the condensate will be carried away by the steam velocity. A proper pocket at the lowest part of the pipe line into which the condensate can drop of at least 100mm diameter is needed in such cases.

Figures below show the wrong and the correct practices in providing the drain points on the steam lines.



Pipe Sizing

The pipes leading to and from steam traps should be of adequate size. This is particularly important in the case of thermodynamic traps, because their correct operation can be disturbed by excessive resistance to flow in the condensate pipe work. Pipe fittings such as valves, bends and tees close to the trap will also set up excessive backpressures in certain circumstances.

Air Binding

When air is pumped into the trap space by the steam, the trap function ceases. Unless adequate provision is made for removing air either by way of the steam trap or a separate air vent, the plant may take a long time in warming up and may never give its full output.

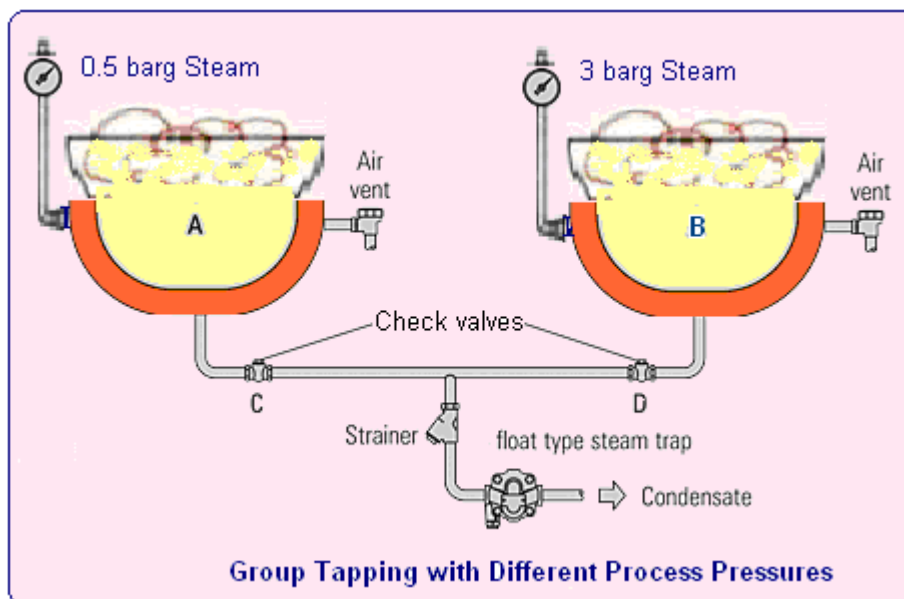
Steam Locking

The possibility of steam locking can sometimes be a deciding factor in the selection of steam traps. This is similar to air binding except that the trap is locked shut by steam instead of air. It can occur whenever a steam trap is fitted remotely from the plant being drained. It can become acute when condensate is removed through a siphon or dip pipe. To relieve this problem a trap is provided with a 'steam lock release' valve. This is an internal needle valve which allows the steam locked in the siphon pipe to be bled away past the main valve. Because the needle valve is just open enough to avoid steam wastage it has a limited capacity to vent air. Traps of this type are often provided with combined air vents and steam lock release.

The typical example is a drying cylinder. It is always advisable to use a float trap provided with a steam lock release arrangement. Other types of traps will open and eventually cope with a steam lock, however, the drainage and plant performance will be erratic. This is clearly unacceptable to users of process plant where batch times, quality and efficiency are of high importance.

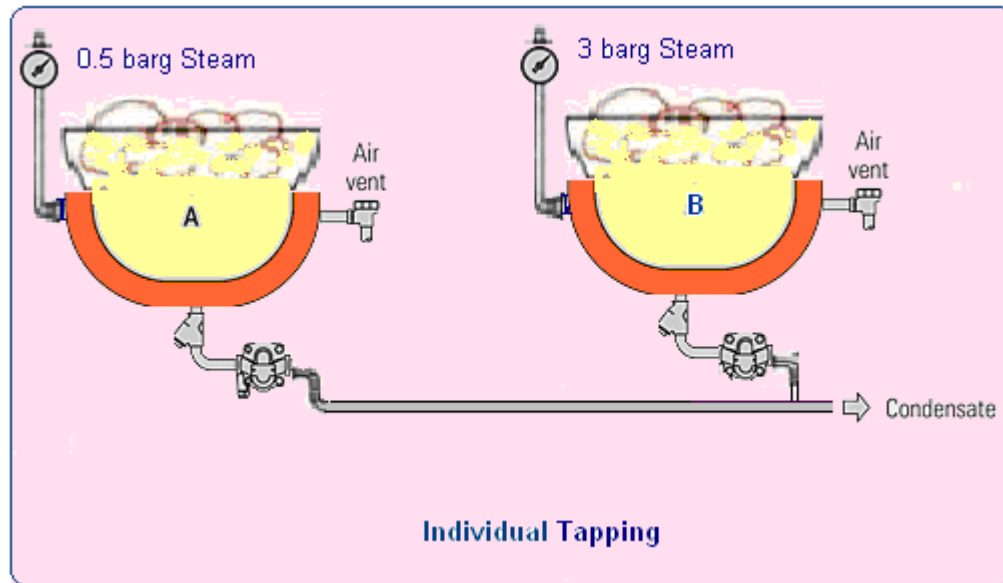
Group Trapping vs. Individual Trapping

Group trapping describes the use of one trap serving more than one application as shown in figure below. This is known as group trapping. No doubt it saves money, but it is rarely successful, since it normally causes water-logging and loss of output.

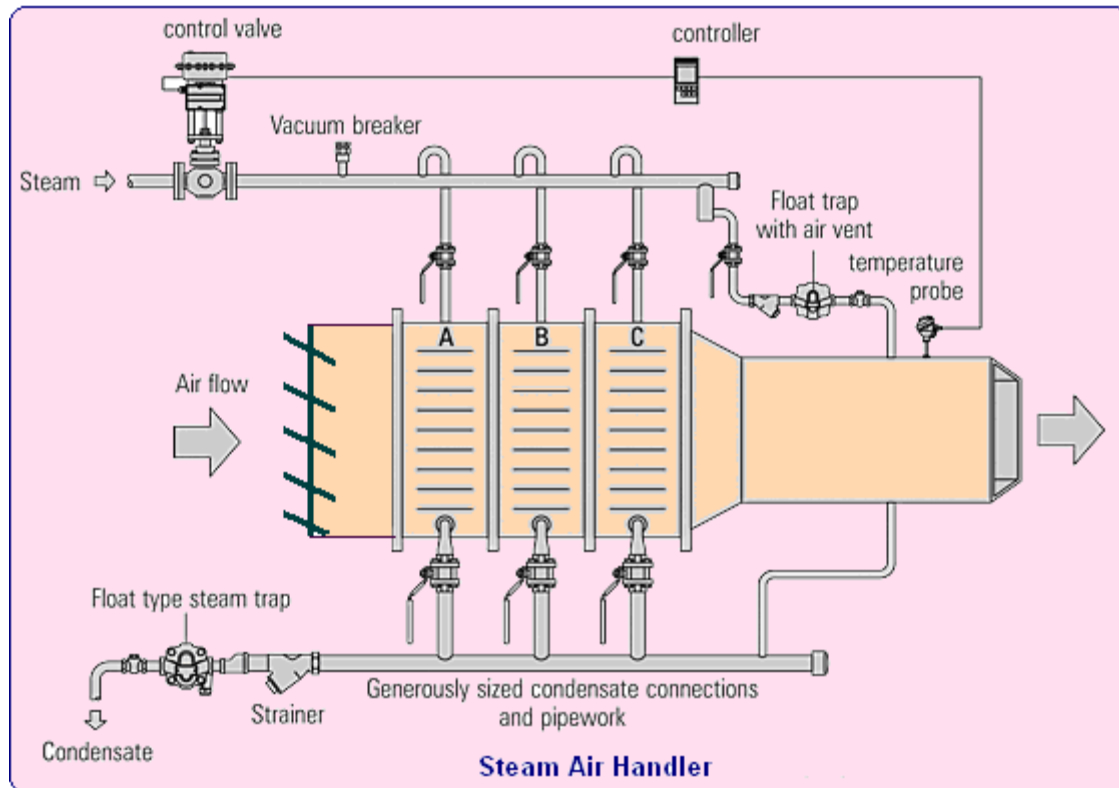


The steam consumption of a number of units is never the same at a moment of time and therefore, the pressure in the various steam spaces will also be different. Figure above shows two batch processes (jacketed pans) operating at two different steam pressures with the drain line from each connected to one steam trap. The higher pressure in plant B will allow condensate

from this vessel to drain but will stop condensate being discharged from plant A as check valve C will be held closed. Plant A will waterlog and will suffer a severe drop in performance. The only satisfactory arrangement, thus would be to drain each steam space with own trap and then connect the outlets of the various traps to the common condensate return main as shown in figure below



One possible application suitable for group trapping is an HVAC air handling unit with multiple heater sections in series. The figure shows 3 steam coils fed with one control valve. This 'flow' type application differs from the batch (or non-flow) process described earlier. The heater sections will always share any load change as they are served by the same control valve.



Note that this scheme shall only work where all sections are fed by one control valve and the same secondary fluid is being heated by all sections. In any case, with the low cost of steam traps available today, it is always better for steam using equipment to be trapped on an individual basis rather than on a group basis.

Dirt

Dirt is the common enemy of steam traps and the causes of many failures. Pipe dirt created during installation contain scale, castings, weld metal, piece of packing and jointing materials, etc. When the system has been in use for a while, the inside of the pipe work and fittings, which are exposed to corrosive condensate, can get rusted. Thus, rust in the form of a fine brown powder is also likely to be present. All this dirt will be carried through the system by the steam and condensate until it reaches the steam trap. Some of it may pass through the trap into the condensate system without doing any harm, but some dirt will eventually jam the trap mechanism. It is advisable to use a strainer positioned before the steam trap to prevent dirt from passing into the system. Float-thermostatic steam traps are quite resistant to dirt due to the low velocity flow through a relatively large orifice.

Water Hammer

Water hammer is a symptom of a problem in the steam system. This could be due to poor design of the steam and condensate pipe work, the use of the wrong type of trap/s or a leaking steam trap, or a combination of these factors.

A water hammer in a steam system is caused by condensate collection in the plant or pipe work picked up by the fast moving steam and carried along with it. When this collection hits obstructions such as bends, valves, steam traps or some other pipe fittings, it is likely to cause severe damage to fittings and equipment and result in leaking pipe joints.

Water hammer can be caused in a number of ways, including:-

- Failure to remove condensate from the path of high velocity steam in the pipe work
- From an application which is temperature controlled and where condensate has to lift to a return line, or return to a pressurized system
- The inability of condensate to properly enter or travel along an undersized return line, due to either (a) flooding, or (b) over-pressurization with the throttling effects of flash steam.

The problem of water hammer can be eliminated by positioning the pipes so that there is a continuous slope in the direction of flow. A slope of at least ½" (12mm) in every 10 ft (3 m) is necessary, as also an adequate number of drain points every 100 to 150 ft (30 to 50 m) with adequately sized drain pockets. The bottom of any riser must also be drained.

If a steam trap persistently fails on an established system due to water hammer, it is probably the fault of the system layout, rather than the trap. It is important that the pipe work is designed and installed correctly. This will help to maintain thermal performance of the system throughout its service life.

Steam trap drainage of temperature controlled processes

The steam trap is an automatic valve that relies on the system dynamics to provide flow. It has to rely on and react to external factors, such as steam pressure or static head pressure on the inlet side of the trap. The outlet pressure must be lower than the inlet pressure to provide flow in the correct direction. *The rate of flow through any steam trap is therefore related to the differential pressure across it.*

It is also possible to have negative differential pressures across the trap, which would promote reverse flow through it. When traps are installed to pass condensate into common return lines, it is advisable to fit non-return valves after each trap to prevent reverse flow under negative pressure conditions.

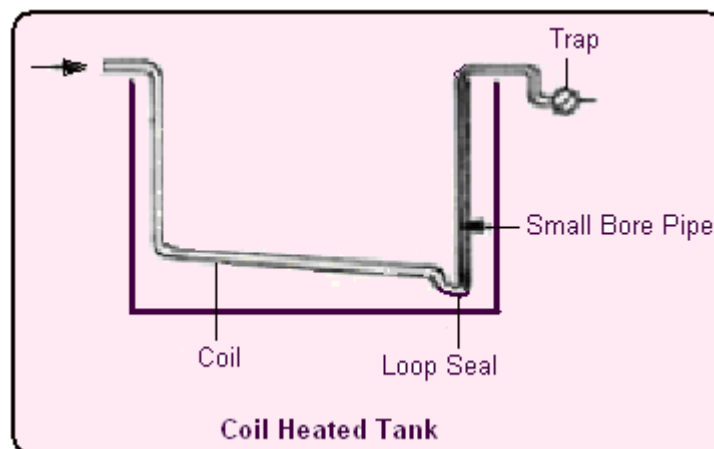
The occurrence of zero and negative differential pressure across steam traps is commonplace. The effects are commonly seen with temperature controlled processes i.e. heater batteries,

calorifiers, jacketed pans, plate heat exchangers, in fact any process that has a control valve on the steam supply. It can occur irrespective of steam supply pressure, and depends wholly on the condensate system pressure and the steam pressure in the heat exchanger.

Whenever it is predicted or diagnosed, another solution, such as a pump-trap is required to remove the condensate from the heat exchanger.

Lifting the condensate

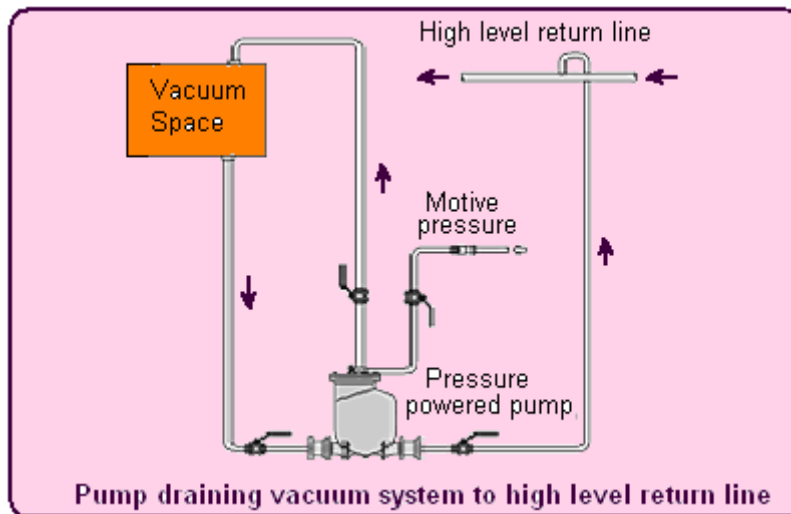
In the interest of energy and treated water savings, every effort should be made to recover and re-use the condensate. Generally, this means lifting the condensate into a return main above the equipment. There may also be a case where the layout of the plant dictates that the steam traps be fitted above the equipment being drained. Wrong installation can lead to trouble. Because of the backpressures imposed upon the steam trap, it is often better not to lift the condensate directly from the trap, but to let it flow by gravity to a pump or a pumping trap, which can then do the lifting. However, if it is decided that the condensate has to be lifted by its own pressure at the trap, it is important to ensure that the installation is correctly arranged. The figure below shows a desirable arrangement of condensate draining and lifting. The rising pipe coil is looped to form a water seal. A small bore pipe is then passed through a steam tight joint at the top of the rising pipe, and its end is pushed well into the loop seal. The trap is fitted as close to the top of this pipe as possible. The water seal now makes it near impossible for the steam to enter the pipe leading up to the trap, and the small bore of this pipe ensures that the water column rises steadily due to steam bubbles.



Special requirements (Vacuum drainage)

Condensate removal from a steam space working under vacuum can be a problem. If a steam trap is used, its outlet must be connected to a source of greater vacuum than that in the steam space to ensure a constant differential pressure across the orifice to discharge the condensate.

Where this is not possible, a pressure powered pump can be used to drain condensate from the plant.



A soft seated check valve is recommended on the pump outlet where little or no lift is present, and an air break will act as an anti-siphoning device when draining to a point below the pump. Should the pump be draining condensate from a vacuum gas system then compressed air or inert gas can be used as the motive force to drive the pump.

Maintenance of Steam Traps

Dirt is one of the most common causes of steam traps blowing steam. Dirt and scale are normally found in all steam pipes. Bits of jointing material are also quite common. Since steam traps are connected to the lowest parts of the system, sooner or later this foreign matter finds its way to the trap. Once some of the dirt gets logged in the valve seat, it prevents the valve from shutting down tightly thus allowing steam to escape. The valve seal should therefore be quickly cleaned, to remove this obstruction and thus prevent steam loss.

In order to ensure proper working, steam traps should be kept free of pipe-scale and dirt. The best way to prevent the scale and dirt from getting into the trap is to fit a strainer. Strainer is a detachable, perforated or meshed screen enclosed in a metal body. It should be borne in mind that the strainer collects dirt in the course of time and will therefore need periodic cleaning. It is of course, much easier to clean a strainer than to overhaul a steam trap.

Routine maintenance

In most industries, maintenance of steam traps is not a routine job and is neglected unless it leads to some definite trouble in the plant. In view of their importance as steam savers and to monitor plant efficiency, the steam traps require considerably more care than is given. One may consider a periodic maintenance schedule to repair and replace defective traps in the shortest

possible time, preferable during regular maintenance shut downs in preference to break down repairs.

Routine maintenance depends on the type of trap and its application. The steam trap must be checked from time to time and any routine maintenance should include the renewal of any suspect parts, if it is to be cost effective.

The elements of thermostatic traps can generally be changed by removing a screwed in seat. Replacement is simple and the remade trap will be reliable assuming the maintenance instructions are correctly carried out.

The weakest point is often the joint between trap body and seat, particularly if this has been allowed to blow steam. If the seat or disc faces of a thermodynamic trap become damaged, the disc can simply be replaced. Damage to seating faces can be rectified by lapping gently.

Replacing the seats of some higher pressure thermodynamic traps is more complicated.

Always check with the manufacturer regarding the correct technique for any maintenance work required on steam traps.

Replacement of traps

On occasions, it will be easier and cheaper to replace traps rather than repair them. In these cases it is essential that the traps themselves can be changed easily. Flanged connections provide one solution, although the flanged trap is more expensive than the equivalent screwed trap. Mating flanges are an additional expense. A swivel connector allows rapid easy removal and replacement of the sealed trap.

Performance Testing of Steam Traps

Steam trap performance assessment is basically concerned with answering the two questions:

- 1) Is the trap working correctly or not?
- 2) If not, has the trap failed in the open or closed position?

Traps that fail 'open' result in a loss of steam and its energy. Where condensate is not returned, the water is lost as well. The result is significant economic loss, directly via increased boiler plant costs, and potentially indirectly, via decreased steam heating capacity.

Traps that fail 'closed' do not result in water losses, but can result in significantly reduced heating capacity and/or damage to steam heating equipment.

A major problem has always been the accurate identification of faulty traps. Wrong diagnosis can allow faulty traps to remain troublesome, and perfectly sound traps to be replaced unnecessarily. Accurate diagnosis is therefore important to any maintenance program.

Various diagnostic methods have included listening devices, optical sight glasses, temperature

monitoring, and ultrasonic techniques. All of these can give an indication of flow, but become inaccurate as system conditions change.

Sight glasses: Sight glasses are useful in ascertaining the proper functioning of traps and in detecting leaking steam traps. In particular, they are of considerable advantage when a number of steam traps are discharging into a common return line. If it is suspected that one of the traps is blowing steam, it can be quickly identified by looking through the sight glass.

Sight glasses offer a partial solution, especially the combined sight/check valve that gives a visual indication of flow plus a non-return facility, however, glasses will require changing occasionally.

Sound Method: Mechanisms within steam traps and the flow of steam and condensate through steam traps generate sonic (audible to the human ear) and supersonic sounds. However, noise level will vary with disturbance from adjacent traps, and condensate load. Interpretation of signals is difficult even for experienced operators. Proper listening equipment, coupled with the knowledge of normal and abnormal sounds, can yield reliable assessments of steam trap working condition. Listening devices range from a screwdriver or simple mechanic's stethoscope that allow listening to sonic sounds.

A modern version of the listening rod is the ultrasonic trap tester which detects ultrasound generated by a leaking trap. It is, unfortunately, unable to differentiate between live steam and flash steam passing through the trap. It is also unable to detect the subtle differences explained above.

Temperature Method: Saturated steam and condensate exist at the same temperature. So it's not possible to distinguish between the two based on temperatures. Still, temperature measurement provides important information for evaluation purposes.

A cold trap (i.e., one that is significantly cooler than the expected saturated steam temperature) indicates that the trap is flooded with condensate, assuming the trap is in service. On the other hand, the temperature downstream of the trap will be nearly constant, if significant steam is getting past the trap.

As it is perfectly feasible for condensate and steam to coexist at the same temperature in the same system, it makes accurate diagnosis difficult on temperature alone.

For hydrocarbon and processing industries that requires continuous monitoring of processes, an integrated steam trap testing device consisting of a sensor, fitted inside the steam trap, and capable of detecting the physical state of the medium at that point by conductivity is a reliable

method to predict blockages. It is not affected by flash steam disturbance. The result is finite and not subject to interpretation. The sensors can be integral to the trap or are available in separate sensor chambers.

Energy Assessment of Steam Traps

The international standard ISO 7841 describes a reliable and accurate test methodology for losses from any type of steam trap. Energy can be lost through the trap but this may depend on size, type and the load. The energy loss is primarily at no load conditions and is negligible as the condensate load increases. Energy will be lost from the trap due to radiation but this can be reduced considerably by lagging.

A comparison of the inherent energy requirements of the main steam traps is as follows:

Thermostatic steam traps

Under normal operating conditions, the thermostatic trap holds back condensate until it has cooled to a certain temperature. Steam does not reach the main valve so there is no apparent steam wastage. However, water logging of plant can lead to reduced output and extended operating times. More steam may be required although this will not appear as an energy requirement attributable to the steam trap.

In some cases a cooling leg may be incorporated so that the steam space is kept clear of condensate. Energy is thereby lost due to radiation from the cooling leg and from the trap body. This in itself creates an additional condensate load, but there is no passage of live steam through the trap.

The situation can change under no-load conditions. Heat loss from the trap body cools the condensate surrounding the element which then opens. The minimal amount of condensate involved is discharged and is then replaced by steam. Laboratory tests indicate typical losses up to 0.5 kg/hr. *Any attempt to lag a thermostatic trap will result in a serious delay in the opening of the trap. Severe water logging will result and hence lagging is not recommended for thermostatic traps.*

Mechanical steam traps

The float-thermostatic trap is another example where the valve and seat are normally flooded and there is no steam loss through the trap. Conversely, the float-thermostatic trap is relatively large in size, and there may be a noticeable loss from the trap caused by radiation.

The float-thermostatic trap can be lagged to reduce heat losses and this will not affect its operation. *Insulation lagging is normally recommended on outdoor applications to minimize the*

danger of damage due to freezing when steam might be turned off.

The inverted bucket trap has surprisingly little in common with the float type trap. The trap closes when steam enters and bubbles through into the bucket to make it buoyant. It will not open until the steam has been dissipated. This will occur as the steam leaks away through the hole in the bucket which serves as an air vent. The steam will collect in the top of the trap itself and when the main valve opens, this steam is vented.

Laboratory tests indicate losses of around 0.5 kg/h for ½" traps under these low load conditions. However, there is additional radiation loss from the body, which can be quite large. Lagging is sometimes recommended but the heat loss and its resulting condensate will be much the same as an equivalent float type trap.

Thermodynamic steam traps

The thermodynamic trap has the great simplicity in that it either works correctly or fails. The operation depends on condensate approaching steam temperature, producing flash steam at the orifice and causing the trap to close. It does this with condensate on the upstream side and again the flooded valve means that there can be no loss through the trap. However the trap will open periodically as heat is lost from the cap.

Under no-load conditions, i.e. when condensate is being produced only by heat loss from the upstream pipeline, the condensate on the upstream side may exhaust and the trap will then require a small amount of live steam to cause it to close. Much will depend on ambient conditions but the loss will generally be around 0.5 kg/h and this could be doubled in severe weather. The tests have shown that radiation losses are not more than 0.25 kg/h which is at least a quarter of that experienced by equal sized inverted bucket traps. Conversely, such losses can be halved by simply fitting an insulating cover over the top cap.

Energy Saving Opportunities

Monitoring Steam Traps

For testing a steam trap, there should be an isolating valve provided in the downstream of the trap and a test valve shall be provided in the trap discharge. When the test valve is opened, the following points have to be observed:

- Condensate discharge-Inverted bucket and thermodynamic disc traps should have intermittent condensate discharge. Float and thermostatic traps should have a continuous condensate discharge. Thermostatic traps can have either continuous or intermittent discharge depending upon the load. If inverted bucket traps are used for extremely small load, it will have a continuous condensate discharge.

- Flash steam-This shall not be mistaken for a steam leak through the trap. The users sometimes get confused between a flash steam and leaking steam. The flash steam and the leaking steam can be approximately identified as follows:
 - If steam blows out continuously in a blue stream, it is a leaking steam.
 - If a steam floats out intermittently in a whitish cloud, it is a flash steam.
 - 2) Continuous steam blow and no flow indicate there is a problem in the trap. Whenever a trap fails to operate and the reasons are not readily apparent, the discharge from the trap should be observed. A step-by-step analysis has to be carried out mainly with reference to lack of discharge from the trap, steam loss, continuous flow, sluggish heating, to find out whether it is a system problem or the mechanical problem in the steam trap.
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Avoiding Steam Leakages

Failed steam traps can be a source of steam leakage that must be avoided. Just to give a glimpse of energy loss, a 3 mm diameter hole on a pipeline carrying 7 kg/cm^2 Steam would waste 33 KL of fuel oil per year. Steam leaks on high-pressure mains are prohibitively costlier than on low pressure mains. Any steam leakage must be quickly attended to. In fact, the plant should consider a regular surveillance program for identifying leaks through the traps. Indeed, by plugging all leakages, one may be surprised at the extent of fuel savings, which may reach up to 5% of the steam consumption in a small or medium scale industry or even higher in installations having several process departments.

To avoid leaks it may be worthwhile considering replacement of all defective steam traps. The payback is very quick usually less than a year.

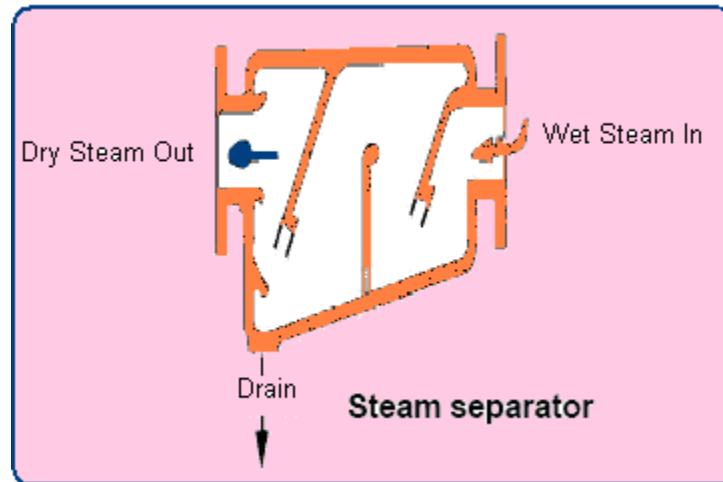
Providing Dry Steam for Process

The best steam for industrial process heating is the dry saturated steam. Wet steam reduces total heat in the steam. Also water forms a wet film on heat transfer and overloads traps and condensate equipment. Super heated steam is not desirable for process heating because it gives up heat at a rate slower than the condensation heat transfer of saturated steam.

It must be remembered that a boiler without a superheater cannot deliver perfectly dry saturated steam. At best, it can deliver only 95% dry steam. The dryness fraction of steam depends on various factors, such as the level of water to be a part of the steam. Indeed, even as simple a thing as improper boiler water treatment can become a cause for wet steam.

As steam flows through the pipelines, it undergoes progressive condensation due to the loss of heat to the colder surroundings; the extent of the condensation depends on the effectiveness of the lagging. For example, with poor lagging, the steam can become excessively wet.

Since dry saturated steam is required for process equipment, due attention must be paid to the boiler operation and lagging of the pipelines. In addition to placing steam traps through out the distribution network, a steam separator may be installed on the steam main as well as on the branch lines to reduce wetness in steam and improve the quality of the steam going to the units. By change of direction of steam, steam separators causes the entrained water particles to be separated out and delivered to a point where they can be drained away as condensate through a conventional steam trap.



Flash steam

An effect caused by passing hot condensate from a high pressure system to a low pressure system is the naturally occurring phenomenon of flash steam. This can confuse the observer regarding the condition of the steam trap.

The low pressure steam produced is usually referred to as 'flash steam'. The amount of 'flash' steam released can be calculated by the following relation with the help of steam tables:

$$\text{Flash Steam Available \%} = (S1 - S2) / L2$$

Where

S1 is the sensible heat of higher pressure condensate

S2 is the sensible heat of the steam at lower pressure (at which it has been flashed)

L2 is the latent heat of the flash steam (at lower pressure)

If the trap were discharging 500 kg/h of condensate at 7 barg to atmosphere, the amount of flash steam generated would be $500 \times 0.134 = 67$ kg/h, equivalent to approximately 38 kW of energy loss!

This represents quite a substantial quantity of useful energy, which is all too often lost from the

heat balance of the steam and condensate loop, and offers a simple opportunity to increase system efficiency if it can be captured and used.

Reliability

Reliability of good steam trapping means optimum performance with the minimum of attention.

Causes of unreliability are often associated with the following:

- Corrosion is a main concern, due to the impurities and dissolved gases (CO₂) of the condensate. This can be countered by using particular materials of construction, and good feed water conditioning.
 - Water hammer, often due to a lift after the steam trap, sometimes overlooked at the design stage and often the cause of unnecessary damage to otherwise reliable steam traps.
 - Dirt, accumulating from a system where water treatment compound is carried over from the boiler, or where pipe debris is allowed to interfere with trap operation
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Codes and Standards

The international codes and standards applicable to the steam traps are listed below:

ISO 6552: 1980:	Glossary of technical terms for automatic steam traps
ISO 6553: 1980:	Marking of automatic steam traps
ISO 6554: 1980:	Face-to-face dimensions for flanged automatic steam traps
ISO 6704: 1982:	Classification of automatic steam traps
ISO 6948:1981:	Production and performance characteristic tests for steam traps
ISO 7841: 1988:	Methods for determination of steam loss of automatic steam traps
ISO 7842: 1988:	Methods for determination of discharge capacity of steam traps
